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Europäisches Patentamt

JUL 13 1998



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EP 0 784 352 A1

(12)

EUROPEAN PATENT APPLICATION

published in accordance with Art. 158(3) EPC

- (43) Date of publication: 16.07.1997 Bulletin 1997/29
- (21) Application number: 96922230.6
- (22) Date of filing: 04.07.1996

- (51) Int. Cl.⁶: H01M 8/02
- (86) International application number: PCT/JP96/01859
- (87) International publication number: WO 97/02612 (23.01.1997 Gazette 1997/05)

- (84) Designated Contracting States: **DE FR GB**
- (30) Priority: 05.07.1995 JP 194333/95
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(54) SEPARATOR FOR FUEL CELLS OF SOLID POLYELECTROLYTE TYPE AND PROCESSES OF THE PRODUCTION THEREOF

(57)A separator for fuel cells of solid polyelectrolyte type which overcomes the disadvantages of the prior art, is lightweight, can be slotted easily, and exhibits high gas barrier properties; and processes for the production thereof. The separator is of the type to be sandwiched between gas diffusion electrodes of the fuel cell and characterized by being made of the carbonaceous composite material comprising expanded graphite particles which have a mean particle diameter of 5 to 12 µm and at least 80 % of which have diameters falling within the range of 0.1 to 20 µm and a thermoplastic or thermosetting resin or a sinter thereof, wherein the graphite particles are dispersed in the resin of sinter thereof, and having slots for feeding oxidant gas or fuel gas on one or both surfaces thereof. The separator can be produced by mixing a thermoplastic or thermosetting resin with the above-specified expanded graphite particles, pressure-molding the obtained mixture at ordinary temperature to 400 °C and forming slots of feeding oxidant gas or fuel gas on one or both surfaces of the resulting carbonaceous composite material, or by mixing a thermosetting resin with the above graphite particles, pressuremolding the obtained mixture at ordinary temperature to 400 °C, firing the resulting molding in a nonoxidizing atmosphere at 700 to 3000 °C to form a carbonaceous composite material, and forming slots for feeding oxidant gas or fuel gas on one or both surfaces of the material, or by mixing a thermosetting resin with the above graphite particles, pressure-molding the obtained



rature to 400 °C, forming slots fuel gas on one or both surling, and firing the resulting zing atmosphere at 700 to

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Technical Field

The present invention relates to a separator for polymer electrolyte fuel cells and processes for production thereof.

Background Art

Fuel cells have excellent features such as (1) it is virtually unnecessary to use any fossil fuel which may be exhausted in a not far future, (2) substantially no noise is produced in electricity generation, and (3) energy recovery is high as compared with the cases of other methods of electricity generation; therefore, utilization of fuel cells in relatively small power plant at building or factory is being studied.

Of fuel cells, polymer electrolyte fuel cells operate at low temperatures and have no problem of corrosion of cell parts, as compared with other type fuel cells and, moreover, can generate a relatively large electric current at low operating temperatures; therefore, polymer electrolyte fuel cells are drawing attention as a substitute for internal combustion engine of automobile.

In polymer electrolyte fuel cells, the separator used therein as one component has roles of (a) providing a passage of a reactive gas fed into the fuel cell, (b) transmitting the electricity generated in the fuel cell, to outside, and (3) dissipating the heat generated in the fuel cell. In order to perform these roles, the separator must satisfy requirements of light-weightness, high gas barrier property and easy cuttability for groove formation.

The separator used in polymer electrolyte fuel cells has heretofore been made of graphite impregnated with a resin (e.g. phenolic resin) or graphite having a glassy carbon layer formed thereon, in view of their processability and cost.

The graphite impregnated with a resin is expensive because a step of impregnation and drying must be repeated a plurality of times in order to allow said graphite to have a desired gas barrier property; further, said graphite has a high density because of the high density of graphite, making large the total weight of fuel cell.

The graphite having a glassy carbon layer formed thereon requires a complicated process and is expensive because a step of impregnation and drying is repeated a plurality of times as in the case of the graphite impregnated with a resin and then is fired in a non-oxidizing atmosphere; further, said graphite has a high density because of the high density of graphite, making large the total weight of fuel cell.

It is considered to use glassy carbon as a material for separator, as done in phosphoric acid fuel cells. In this case, glassy carbon is lighter than graphite and the total weight of fuel cell is small; however, glassy carbon is expensive and, moreover, fragile, making the groove formation therein very difficult and requiring a high processing cost.

Therefore, it has been necessary to develop a separator for polymer electrolyte fuel cells, which is lightweight, can be grooved easily and has a high gas barrier property.

The object of the present invention is to solve the above-mentioned problems of the prior art and provide (1) a separator for polymer electrolyte fuel cells, which is lightweight, can be grooved easily and has a high gas barrier property and (2) processes for production of such a separator.

Disclosure of the Invention

According to the present invention, there is provided a separator for polymer electrolyte fuel cells, interposed between the gas diffusion electrodes of the fuel cell and having, in at least one side, a groove for supply of an oxidizing agent or a fuel gas, which separator is made of carbon composite material comprising (a) an expanded graphite powder and (b) a thermoplastic resin or a thermosetting resin or a fired product of the thermosetting resin, and the expanded graphite powder (a) being dispersed in the component (b), wherein the expanded graphite powder has an average particle diameter of 5-12 µm and at least 80% of the total particles of the expanded graphite powder have particle diameters of 0.1-20 µm.

According to the present invention, there is further provided a process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting or thermoplastic resin and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 µm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 µm, molding the resulting mixture at a temperature of room temperature to 400°C to obtain carbon composite material, and then, forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the carbon composite material.

According to the present invention, there is further provided a process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting resin and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 µm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 µm, molding the resulting mixture at a temperature of room temperature to 400°C, and firing the molded material at 700-3,000°C in a non-oxidizing atmosphere to obtain carbon composite material, and then, forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the

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carbon composite material; or a process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting resin and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 µm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 µm, molding the resulting mixture at a temperature of room temperature to 400°C to obtain a molded material, and forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the molded material, and then, firing the molded material at 700-3,000°C in a non-oxidizing atmosphere.

The present inventors made a study in order to achieve the above object and found out that expanded graphite having particular particle diameters has excellent miscibility with a thermosetting or thermoplastic resin. Based on an idea that when a mixture of such expanded graphite and a thermosetting or thermoplastic resin (they have good miscibility) is shaped, there might be obtained a separator for polymer electrolyte fuel cells, which is lightweight, can be grooved easily and has a high gas barrier property, the present inventors made a further study. As a result, the present invention has been completed.

Best Mode for Carrying out the Invention

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The present invention is hereinafter described in detail.

The expanded graphite used in the present invention has no particular restriction as to the raw material. The raw material can be any raw material ordinarily used in production of expanded graphite, such as natural graphite, pyrolytic graphite, Kish graphite or the like.

Production of expanded graphite from the above raw material can be conducted by a known process. For example, concentrated sulfuric acid is mixed with hydrogen peroxide to form peroxomonosulfuric acid; thereto is added raw material graphite with stirring to give rise to a reaction for about 1 hour to 1 day; and the reacted graphite is heated at 500-1,000°C in an inert gas.

Incidentally, the expanded graphite used in the present invention may be expanded graphite obtained by adding, in the above production of expanded graphite using concentrated sulfuric acid and hydrogen peroxide, at least one oxidizing agent selected from perchloric acid, a perchloric acid salt and ammonium hydrogenperoxodisulfate [Japanese Patent Application Kokai (Laid-Open) No. 16406/1994]. It specifically is expanded graphite obtained by adding 15% of ammonium hydrogenperoxodisulfate to a mixture of 320 parts by weight of 95 wt. % concentrated sulfuric acid and 4 parts by weight of 62% hydrogen peroxide, mixing them with cooling to 20°C or lower, adding natural graphite to the mixture to give rise to a reaction for 24 hours, and firing the reaction product up to 1,000°C in nitrogen gas.

The expanded graphite produced as above is ground and as necessary allowed to have a desired particle size and desired particle diameters. The expanded graphite used in the present invention must have an average particle diameter of 5-12 μ m and at least 80% of the total particles of the graphite powder must have particle diameters of 0.1-20 μ m.

When the average particle diameter of the expanded graphite used in the present invention is smaller than 5 μ m, the penetration of the thermosetting or thermoplastic resin into the gap between expanded graphite particles is difficult, resulting in very low gas barrier property. When the average particle diameter is larger than 12 μ m, the filling of the gap between expanded graphite particles, with the thermosetting or thermoplastic resin is insufficient, resulting in (1) very low gas barrier property and (2) reduced packing density which invites insufficient electrical connection and consequent low electroconductivity.

Further, it is necessary that at least 80% of the total particles of the graphite powder used in the present invention have particle diameters of $0.1-20~\mu m$. In general, expanded graphite which is ground and as necessary allowed to have a desired particle size and desired particle diameters, has a particle size distribution wherein the average particle diameter gives a distribution peak. In the present expanded graphite, however, when its powder total particles are measured for particle size distribution, it is necessary that at least 80% of the powder total particles have particle diameters of $0.1-20~\mu m$ and less than 20% of the powder total particles have particle diameters of smaller than $0.1~\mu m$ or larger than $20~\mu m$.

Needless to say, in the present expanded graphite, the total powder particles may have particle diameters of 0.1-20 µm or of even narrower range.

When the peak of particle size distribution is lower, the total number of particles having particle diameters smaller than 0.1 µm and larger than 20 µm increases. When the peak of particle size distribution moves to either one direction, the number of graphite particles having particle diameters smaller than 0.1 µm or larger than 20 µm increases. When the number of particles having particle diameters smaller than 0.1 µm increases, the surface area of the expanded graphite powder increases, whereby the thickness of the resin present between the expanded graphite particles becomes smaller and the resulting separator has reduced gas barrier property. When the number of graphite particles having particle diameters larger than 20 µm increases, part of the graphite particles may be exposed at the surface of the resulting separator and the number of resin layers formed between the expanded graphite particles is small, giving a separator of low gas harrier property.

The above-mentioned grinding of expanded graphite may be conducted by any known method such as mixer, jet mill, ball mill, pin mill, freeze-grinding or the like. Allowing ground expanded graphite to have a desired particle size and

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shown in Table 5, in an inert gas atmosphere. The separators for polymer electrolyte fuel cells were produced using obtained fired material, and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 5.

Table 5

	Example		
	5-1	5-2	5-3
Firing temperature(°C)	1000	2000	2500
Expanded graphite	100	100	100
Resin			
Polycarbodiimide	100	100	100
Phenol			
Polypropylene			
Polytetrafluoroethylene			
Density	1.38	1.42	1.3
Nitrogen gas permeability (cm³cm⁻²min⁻¹atmN₂)	8x10 ⁻⁶	2x10 ⁻⁶	8x10 ⁻⁶
Groove formability	Good	Good	Good

Comparative Example 1

Expanded graphite (its average particle diameter was 100 μm and 20% of the powder total particles had particle diameters of 0.1-20 μm) and a polycarbodiimide resin were mixed in a composition shown in Table 6. The mixture was molded at 150°C at a pressure of 100 kg/cm². The separators for polymer electrolyte fuel cells were produced using obtained molded material, and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 6.

Comparative Example 2

The molded material used in Comparative 1 was fired up to 1,000°C in nitrogen gas. The separators for polymer electrolyte fuel cells were produced using obtained molded material, and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 6.

Comparative Example 3

Expanded graphite (its average particle diameter was 0.5 μm and 20% of the powder total particles had particle diameters of 0.1-20 μm) and a polycarbodiimide resin were mixed in a composition shown in Table 6. The mixture was molded at 150°C at a pressure of 100 kg/cm². The separators for polymer electrolyte fuel cells were produced using obtained molded material, and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 6.

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Table 6

	Comparative Examples		
	1	2	3
Firing temperature(°C)	No firing	1000	No firing
Expanded graphite	100	100	100
Resin(polycarbodiimide)	10	100	1000
Density	1.25	1.21	1.23
Nitrogen gas permeability (cm³cm⁻²min⁻¹atmN₂)	0.2	1	0.3
Groove formability	Good	Good	Fragile and impossible to groove

Comparative Example 4

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Graphites having a density of 2.0 g/cm³ or 1.7g/cm³ were impregnated with a polycarbodiimide resin. The separators for polymer electrolyte fuel cells were produced using the graphites and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 7.

Table 7

	Comparative Examples		
	4-1	4-2	
Firing temperature(°C)	No firing	No firing	
Density	1.7	2	
Nitrogen gas permeability (cm³cm⁻²min⁻¹atmN₂)	90	0.4	
Groove formability	Good	Good	

Comparative Example 5

Grooved graphites having a density of 1.7 g/cm³ or 2.0 g/cm³ were coated with a polycarbodiimide resin and then fired at 1,500°C in a nitrogen gas atmosphere. The separators for polymer electrolyte fuel cells were produced using the grooved graphites and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 8.

Table 8

	Comparative Examples	
	5-1	5-2
Firing temperature(°C)	1500	No firing
Density	1.7	2
Nitrogen gas permeability (cm ³ cm ⁻² min ⁻¹ atmN ₂)	9	4x10 ⁻⁵
Groove formability	Good	Good

*Comparative Example 6

The separators for polymer electrolyte fuel cells were produced using glassy carbon having a density of 1.5/cm³ and the separators were measured for density, gas permeability and groove formability in the same manners as in Example 1. The results are shown in Table 9.

Table 9

	Comparative Examples
	6
Firing temperature(°C)	No firing
Density	1.5
Nitrogen gas permeability (cm ³ cm ⁻² min ⁻¹ atmN ₂)	1x10 ⁻⁷
Groove formability	Groove was broken during grooving.

Industrial Applicability

The present invention provides a separator for polymer electrolyte fuel cells, interposed between the gas diffusion electrodes of the fuel cell and having, in at least one side, a groove for supply of an oxidizing agent or a fuel gas, which separator is made of carbon composite material comprising (a) an expanded graphite powder and (b) a thermoplastic resin or a thermosetting resin or a fired product of the thermosetting resin, and the expanded graphite powder (a) being dispersed in the component (b), wherein the expanded graphite powder has an average particle diameter of 5-12 µm and at least 80% of the total particles of the expanded graphite powder have particle diameters of 0.1-20 µm. The separator for polymer electrolyte fuel cells of the present invention is lightweight, can be grooved easily, and has a high gas barrier property.

Claims

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- 1. A separator for polymer electrolyte fuel cells, interposed between the gas diffusion electrodes of the fuel cell and having, in at least one side, a groove for supply of an oxidizing agent or a fuel gas, which separator is made of carbon composite material comprising (a) an expanded graphite powder and (b) a thermoplastic resin or a thermosetting resin or a fired product of the thermosetting resin, and the expanded graphite powder (a) being dispersed in the component (b), wherein the expanded graphite powder has an average particle diameter of 5-12 μm and at least 80% of the total particles of the expanded graphite powder have particle diameters of 0.1-20 μm.
- 2. A process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting or thermoplastic resin and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 µm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 µm, molding the resulting mixture at a temperature of room temperature to 400°C to obtain carbon composite material, and then, forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the carbon composite material.
- 3. A process according to Claim 2, wherein an amount ratio of the expanded graphite powder and the thermosetting or thermoplastic resin is 10-1,000 parts by weight of the resin per 100 parts by weight of the expanded graphite powder.
- 4. A process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting resin and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 μm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 μm, molding the resulting mixture at a temperature of room temperature to 400°C, and firing the molded material at 700-3,000°C in a non-oxidizing atmosphere to obtain carbon composite material, and then, forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the carbon composite material.
- 5. A process for producing a separator for polymer electrolyte fuel cells, which comprises mixing a thermosetting resin

and an expanded graphite powder, said expanded graphite powder having an average particle diameter of 5-12 µm and at least 80% of the total particles of said expanded graphite powder having particle diameters of 0.1-20 µm, molding the resulting mixture at a temperature of room temperature to 400°C to obtain a molded material, and forming a groove for supply of an oxidizing agent or a fuel gas on at least one side of the molded material, and then, firing the molded material at 700-3,000°C in a non-oxidizing atmosphere.

- 6. A process according to Claim 4 or 5, wherein an amount ratio of the expanded graphite powder and the thermosetting or thermoplastic resin is 10-1,000 parts by weight of the resin per 100 parts by weight of the graphite powder.
- 7. A process according to Claim 4 or 5, wherein the firing in a non-oxidizing atmosphere is conducted at 1,000-2,500 °C.

' INTERNATIONAL SEARCH REPORT

International application No.

PCT/JP96/01859

A. CLASSIFICATION OF SUBJECT MATTER			
	t. C16 H01M8/02		
According to International Patent Classification (IPC) or to both national classification and IPC			
	ELDS SEARCHED		
	documentation searched (classification system followed	by classification symbols)	
111	C1 ⁶ H01M8/02		
Document	ation searched other than minimum documentation to the	extent that such documents are included in the	ne fields searched
Jit	suyo Shinan Koho	1926 - 1996	
KO)	kai Jitsuyo Shinan Koho Toku Jitsuyo Shinan Koho	1971 - 1996 1994 - 1996	
	data base consulted during the international search (name	of data base and, where practicable, search t	erms used)
C. DOC	UMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where	appropriate, of the relevant passages	Relevant to claim No.
A	JP, 01-154467, A (Hitachi,	I.t.d. \	1 - 7
••	June 16, 1989 (16. 06. 89)		1 - /
	Claims 1 to 3; page 3, low	er right column,	•
	lines 13 to 19 (Family: no	ne)	٠.
A	JP, 01-311570, A (Hitachi	Chemical Co., Ltd.).	1 - 7
	December 15, 1989 (15. 12.		
	Claim 1; page 2, upper rig		
	lower left column, line 1	(Family: none)	
A	JP, 60-090807, A (Kobe Stee	el. Ltd.).	1 - 7
	May 22, 1985 (22. 05. 85),	22, 2001,	
	Page 5, upper left column,	line 13 to upper	
	right column, line 16; page column, lines 12 to 15 & Di	e 5, lower left	
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	March 16, 1987 (16. 03. 87)	line 14 to lower	
	Page 2, upper right column left column, line 1; page 5	o, lower right column,	
X Furth	er documents are listed in the continuation of Box C.		
	Categories of cited documents:	"I" later document published after the inter	
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document published prior to the international filing date but inter than the priority date claimed "&" document member of the same patent family			
ate of the actual completion of the international search Date of mailing of the international search report			
Sep	cember 30, 1996 (30. 09. 96)	October 8, 1996 (0)	3. 10. 96)
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INTERNATIONAL SEARCH REPORT

International application No.

PCT/JP96/01859

tegory*	ation). DOCUMENTS CONSIDERED TO BE RELEVANT Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.	
	line 19 to page 3, upper left column, line 16 (Family: none)	1 - 7	
A	JP, 04-214072, A (Osaka Gas Co., Ltd.), August 5, 1992 (05. 08. 92), Paragraphs (0030) to (0031) (Family: none)		
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